



Particles Spreading Phenomena in the Case of Glass Thermal Spraying

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The spreading phenomena of particles during thermal spraying are quite difficult to observe given the kinetics of the process. In this work, the splat formation of glass and alumina is theoretically compared, showing that glass transition and low-thermal conductivity yield a higher ratio between cooling and flattening times, which strongly modifies their spreading behavior. Wipe tests show that splash—splat transition temperature can be modified by the glass composition and its subsequent hydrodynamic properties. The detection of peculiar remaining objects, such as fibers and wavelets shows the possibility of “freezing” some phenomena that are totally unobservable with crystalline oxides, except with high-velocity observations.

Keywords cooling, fragmentation, glass, splat, substrate temperature, wavelets

1. Introduction

In spite of its limited thermo mechanical properties in the as-sprayed conditions (low fracture toughness and hardness, low wear and thermal shock resistance), glass may represent an interesting alternative to crystalline oxides when specific applications are required, such as acid resistant hermetic coatings (Ref 1-5), chemically active coatings (Ref 6-8), and decorative (colored) applications (Ref 9-14). The atmospheric thermal spraying of crystalline oxides (APS, flame spraying) is well known for its inter-splat porosity (Ref 15-16), which explains good thermal properties, as well as the difficulty to obtain dense, hermetic coatings. Low Pressure Plasma Spraying (LPPS) is able to yield more dense coatings (Ref 17), but requires higher investment costs. Moreover, the thermal spraying of pigments and colored single oxides yields a restricted spectrum of colors, due to the alterations of redox and crystalline state during in-flight melting (Ref 18). Glass particles are not able to produce dense as-sprayed coatings, but a thermal post treatment may allow to completely seal the coating (Ref 5, 19) and, sometimes, to produce a glass-ceramic material with improved mechanical properties (Ref 20-21). Composite material can be used to further improve these properties, for example with alumina or yttrium stabilized zirconia (YSZ) (Ref 2, 5, 22-24). Moreover, thermal conductivity of glass is very low (1.2 W/m K, when compared to YSZ:

2.7 W/m K and alumina: 7.4 W/m K (Ref 25-26)), which allows the pigments within glass particles to be hardly heated before impinging onto the substrate, while the glass surface is in liquid or viscoelastic state. In some cases, this effect allows to maintain the original color of the pigment.

This low-thermal conductivity, combined with the glass transition property and a low density, give place to very specific splat formation mechanisms.

The flattening of thermally sprayed crystalline oxides or metallic particles has been widely characterized and modeled (Ref 27-30), as well as the relationship between their hydrodynamic properties (viscosity, surface tension versus temperature) and the spreading factor ($\xi = \text{splat diameter/droplet diameter} = a \cdot \text{Re}^b$, see Table 1) and trend to splash ($K = \sqrt{We} \cdot \sqrt{\text{Re}} > 57.7$ (Ref 29)).

However, experimental hydrodynamic information is not always available for molten crystalline oxides, particularly those with a high melting point, which makes it difficult to model the flattening phenomenon. Although the viscosity of slag was successfully modeled (Ref 31) and though alumina (Ref 30) was experimentally characterized, the lack of data led some authors to assume that YSZ has the same behavior as alumina (Ref 32-33). However, Shinoda et al. (Ref 34) yielded an interesting estimation of YSZ viscosity versus temperature by characterizing splat cooling of plasma-sprayed YSZ particles, and assuming that $\xi = 0.83 \cdot \text{Re}^{0.2}$. On the other hand, oxide glass is well understood and modeled: several authors (Ref 35-42) give empiric formulae to estimate viscosity (Vogel-Fulcher-Tamann law) and surface tension versus temperature from their chemical composition by using mixing laws. Their suitability in a wide compositional range helps to predict the processing properties in the glass industry, and could be extended to thermal spraying as well.

Thermal properties are another key aspect to understand the competition between flattening and cooling mechanisms. Though both processes are supposed to be simultaneous (Ref 43), Jones (Ref 44) assumes their sequential character, which allows to calculate the cooling

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Nomenclature			
a,b	Empirical flattening coefficients, dimensionless	T _s	Substrate temperature, °C
c	Wavelets speed, m/s	T _{glazing}	Typical glazing temperature, °C
C _p	Heat capacity of the particle in the liquid phase, J/kg.K	T _{particle}	Particle temperature, °C
D	Initial diameter of the particle, m	T _{transformation}	Change of state temperature, °C
D _{splat}	Splat diameter, m	\mathcal{T}	Period between wavelets, s
e	Flattened film thickness, m	t _{transf}	Cooling time, s
f	Frequency of wavelets, s ⁻¹	t _{splat}	Flattening time, s
F	Degree of fragmentation, dimensionless	U	Spreading velocity, m/s
g	Gravity constant, m/s ²	V	Particle velocity, m/s
K	Sommerfeld number, dimensionless	V _i	Volume of a size class of particles, m ³
l	Wavelength, m	V _{total}	Total volume of particles, m ³
l _C	Critical wavelength value before obtaining gravitational predominance, m	We	Weber number, dimensionless
L	Latent heat of transformation, J/kg	Greek symbols	
\mathcal{L}	Travel distance of wavelets, m	ΔT	Temperature gap between particle and transformation temperatures, °C
\dot{m}	Particles mass flow rate, kg/s	ξ	Spreading factor, dimensionless
N	Number of impinging particles during t _{transf}	ρ	Particle density, kg/m ³
Nu	Nusselt number, dimensionless	λ	Thermal conductivity, W/m K
P	Probability, dimensionless	μ	Particle viscosity, Pa.s
Re	Reynolds number, dimensionless	σ	Surface tension, N/m
S _{splat}	Surface area of splat, m ²	Ξ	Ratio between cooling and flattening time, dimensionless
S _{exposed}	Substrate surface area exposed to impinging particles, m ²	Ψ	Feedstock intrinsic prefactor for Ξ and t _{transf}
T _g	Glass transition temperature, °C	Ω	Wavelet pulsation, rad/s

Table 1 Values of a and b according to several authors (Ref 28, 29)

a	b	Author
1.2941	0.2	Madejski
1.06	0.125	Ohmori
0.5	0.25	Pasandideh-Fard
1	0.2	Trapaga
0.83	0.2	Yoshida
1.04	0.2	Liu
0.925	0.2	Bertagnolli
1.025	0.2	Li
0.43	0.33	Shinoda

time in an easier way, since impinging droplets would completely flatten (their disk surface depending on initial diameter D and on ξ) before transferring their heat into the substrate. Thus, transformation time of the liquid droplet/disk (solidification onto a cold substrate, in the case of Fukumoto et al. (Ref 45); evaporation onto a hot substrate in the case of Liu et al. (Ref 46)) would be calculated as:

$$t_{\text{transf}} = \frac{4\rho \cdot L}{9Nu \cdot \lambda \cdot \Delta T \cdot \xi^4} \cdot D^2 \quad (\text{Eq 1})$$

where $Nu = 3.66$ (Ref 46) and $\Delta T = |T_{\text{particle}} - T_{\text{transformation}}|$. More accuracy would be yielded by replacing L by $(L + C_p \Delta T)$, where C_p is the heat capacity of liquid before its solidification. Therefore, considering $\xi = a \cdot Re^b$, it comes:

$$t_{\text{transf}} = \frac{4}{9Nu \cdot a^4} \cdot \frac{\rho^{0.2} \cdot \mu^{0.8} \cdot (L + C_p \cdot \Delta T)}{\lambda \cdot \Delta T} \cdot \frac{D^{(2-4b)}}{V^{4b}} = \Psi \cdot \frac{D^{(2-4b)}}{V^{4b}} \quad (\text{Eq 2})$$

Flattening time was estimated by Schiaffino et al. (Ref 47) as $t_{\text{splat}} = D/V$ when $We > 1$ and $Re > 1$. Therefore, the ratio between cooling and flattening time would be:

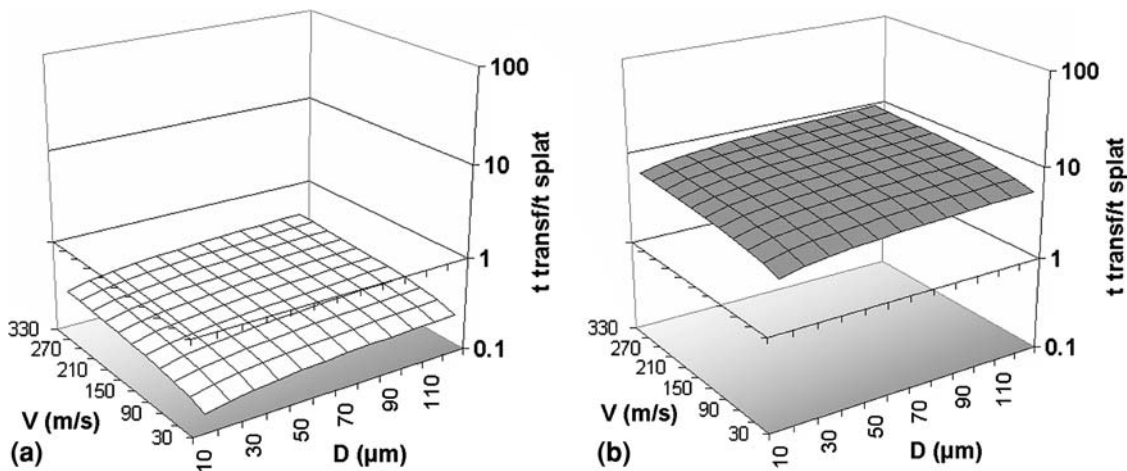
$$\Xi = t_{\text{transf}}/t_{\text{splat}} = \Psi \cdot (D \cdot V)^{1-4b} \quad (\text{Eq 3})$$

The thermal resistance of splat-substrate interface could increase the value of t_{transf} , depending on substrate temperature and on the presence of adsorbates (Ref 48, 49) on its surface. However, assuming similar conditions with respect to this aspect, a comparison of behaviors of impinging droplets of alumina and commercial soda lime silicate container glass can be estimated (Table 2 and Fig. 1). Independently from diameter and velocity, cooling time and value of Ξ of glass particles will be 22 times higher than that of alumina. Therefore, if Jones (Ref 44) hypothesis about sequential flattening and cooling of splats could be questionable for alumina, it appears quite suitable for glasses: this feedstock will remain fluid during a significant lapse of time after flattening. On the other hand, although glass particles are supposed to flatten and splash half as frequently as alumina (Madejski and Sommerfeld prefactors in Table 2 anticipate the intrinsic propensities of both feedstocks), specific phenomena, such as fragmentation, are likely to appear at the edge of the glass splats. Moreover, Li et al. (Ref 50) pointed out that

Table 2 Comparison of flattening and cooling trends of alumina and soda lime silicate glass

Feedstock	Alumina (Ref 26, 30, 53)	Soda lime silicate glass (Ref 7, 25, 35, 41, 54)
ρ (kg/m ³) vs. T (°C)	$2790(1-\alpha \cdot (T-2227))$; $\alpha = 4.22 \cdot 10^{-5}$	$2492(1-3\alpha(T-T_g))$; $\alpha = 1.05 \cdot 10^{-5}$
μ (Pa.s) vs. T (°C)	$2.87 \cdot 10^{-9} \cdot (T+273) \cdot \exp(20500/(T+273))$ $\approx 4.9 \cdot 10^{-3}$ at 3000 °C	$10^{[0.7843+4609.3/(T-234.96)]} \approx 131 \cdot 10^{-3}$ at 3000 °C
σ (N/m) vs. T (°C)	$0.745-0.00004 T \approx 0.35$ at 3000 °C	$0.414-0.000021 T \approx 0.28$ at 3000 °C
λ (W/m K)	7.4	1.2
L (J/kg)	1054000	0
Cp (J/kg.K)	900	600
Madejski prefactor: $(\rho/\mu)^{0.2}$	14	7
Sommerfeld prefactor $(\rho^{0.75}/\mu^{0.5} \cdot \sigma^{0.25})$	1803	937
Ψ	0.80	17.80

All prefactors are estimated at T=3000 °C (see experimentation)

**Fig. 1** Estimation of $\Xi = t_{\text{transf}}/t_{\text{splat}}$ for (a) alumina and (b) soda lime silicate glass particles impinging at T=3000 °C (see experimentation)

incompletely molten particles that impinge onto a substrate have a higher trend to splash, which should be the case for (thermally insulating) glass particles: Thus, splashed and partly unmolten objects can be predicted for glass, from its comparison with alumina.

2. Experimentation

Several commercial glass frits (see Table 3) were hand crushed and planetary milled by Fritsch pulverisette 6, then sieved (40 μm , granulometry measured by Malvern Mastersizer 2000E) and thermally sprayed by APS (Sulzer Metco F4 torch, Ar-H₂: 35-8 slpm, current intensity 500 A, power 18 kW, spraying distance: 100 mm). In-flight temperature and velocity profiles were measured by DPV 2000 (Tecnar Automation, St Bruno, QC, Canada). Particle velocities were measured between 240 and 300 m/s with surface temperatures between 2700 and 3000 °C, depending on their position within the jet. Wipe tests were made in front of AISI 316L polished (0.25 μm) and acetone degreased coupons. A preheating between 170 and 310 °C was performed using hot air and controlled by

optical pyrometry (Land Z5365). Glass splats were subsequently observed by optical microscopy (Nikon Epiphot) and Scanning Electron Microscopy (SEM: Jeol 5800LV), and the perimeter and area of each object were determined by image analysis (45-180 objects studied for each case). The equivalent splat perimeter was established from the splat area, and the degree of fragmentation was calculated as follows:

$$F = \text{Actual splat perimeter/Equivalent perimeter} \\ = \text{Actual perimeter}/\sqrt{(4\pi \cdot \text{area})}$$

Schott (zinc-lead borate), Escol and Cerfav T1 (boro-silicates) glasses which were considered in this study are not completely characterized with respect to their viscosity: Arrhenius approximations ($\log(\mu) = A + B/T$) are possible near their measured characteristic points at low temperatures, but the whole VTF curve ($\log(\mu) = A + B/(T - T_0)$) cannot be obtained. However, they are potentially more fluid than classical soda lime and Cerfav Z5M (low boron) silicate glass at high temperatures. Lower surface tensions are also expected for those glasses, which then should be more likely to splash.

Table 3 Compositions, granulometry, and hydrodynamic information of the studied glass frits

Composition	Soda lime silicate	Cerfav Z5M	Escol ARB342B	Schott G017-209	Cerfav T1
SiO ₂	72.7	70			51.2
B ₂ O ₃	...	2			6.8
Sb ₂ O ₃	...	1			...
Al ₂ O ₃	1	1			1.9
Li ₂ O			4.8
Na ₂ O	14.1	16			10.2
K ₂ O	...	5			...
CaO	8.1	...			11.4
MgO	4.0	...			4.6
BaO	...	2.5			...
ZnO			9.1
d ₁₀ , μm	5.3	4.2	3.6	4.8	3.4
d ₅₀ , μm	19.3	18.9	16.7	17.5	18.5
d ₉₀ , μm	43.4	52.2	50.3	44.8	63.3
Strain point, °C (μ = 10 ^{13.5} Pa.s)	485	518
T _g , °C (μ = 10 ¹² Pa.s)	511	547	453 (a)	416	430-500 (b)
Dilatometric softening point, °C (μ = 10 ^{10.3} Pa.s)	554 (a)	587	489	439 (a)	...
Littleton point, °C (μ = 10 ^{6.6} Pa.s)	673	726	591 (a)	499	500-600 (b)
T _{glazing} (μ = 10 ^{2.3} Pa.s) (°C)	1088	1140	780
μ (3000 °C) (Pa.s)	0.131	0.076
σ (3000 °C) (N/m)	0.28	0.30	0.27	0.22	0.24

(a) Arrhenius approximation from commercial data

(b) Extrapolation of Lakatos formula and qualitative comparison with other commercial glasses

3. Results and Discussion

3.1 Flattening and Cooling Behavior

The spreading factor experimental value ξ of the studied objects (Fig. 2) was calculated as the ratio between the median values of splat (D_{splat}) and particle (d_{50}) diameters. Median and maximum values of degree of fragmentation F (Fig. 3) were compared with the typical values of alumina and zirconia, as measured by Bianchi (Ref 51), Shinoda et al. (Ref 52), and Li et al. (Ref 50). Their evolution with substrate temperature shows that spreading and fragmentation occur more easily on cold substrates, whereas preheating yields lower spreading values than that of alumina. However, the splats seem to be more fragmented than classical oxides, particularly for the highly fusible borate glasses with low surface tension. The high calculated value of $\Xi = t_{\text{transf}}/t_{\text{splat}}$ (Table 4) explains the remaining fluidity of glass after flattening, which allows subsequent fragmentation (flattening splash) that does not occur so easily for YSZ and alumina. At higher temperatures, F appears to be much lower, even for easily fragmented Schott and borosilicate glasses: this could be explained by a better heat transfer onto the substrate (Ref 27). Transition temperatures (splash-splat) of soda lime silicate glass lies under 170 °C, which is comparable with alumina, whereas the other studied glasses seem to keep yielding splashes around 300 °C (Fig. 4).

3.2 Morphology of Splats

Other characteristic aspects of glass splats are visible in Fig. 5-7: unmolten core and peripheral thin film are often observed (see irisation effect in Fig. 5a): This confirms the high-thermal gradient that takes place within glass particles, as studied by Zhang et al. (Ref 3). This gradient was

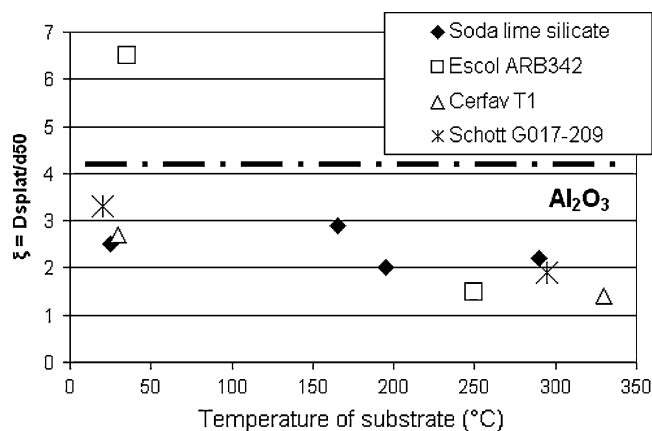


Fig. 2 Spreading factor (ξ) of several glass compositions depending on substrate temperature (T_s), compared with maximum values of alumina splats (after Bianchi (Ref 51))

considered (Ref 50) as a key aspect to predict the high fragmentability of glass splats. The formation of a very thin film is a classical phenomenon at macroscopic scale when excessively fluid glass is blown with too much pressure by a craftsman. Another classical phenomenon, which is seen here at microscopic scale, is the fiberization of the splats, with very long (up to 2 millimeters) fibers (Fig 6a). The observation of such objects usually requires a high velocity camera when crystalline oxides are thermally sprayed (Ref 27). The remaining fluidity after flattening may explain this effect, as well as the beginning of coalescence that is observed between a recently flattened splat and another splat (Fig. 6b). Gawne et al. (Ref 1) report a similar effect at high substrate temperatures with borosilicate glass. This peculiar “slow freezing” behavior

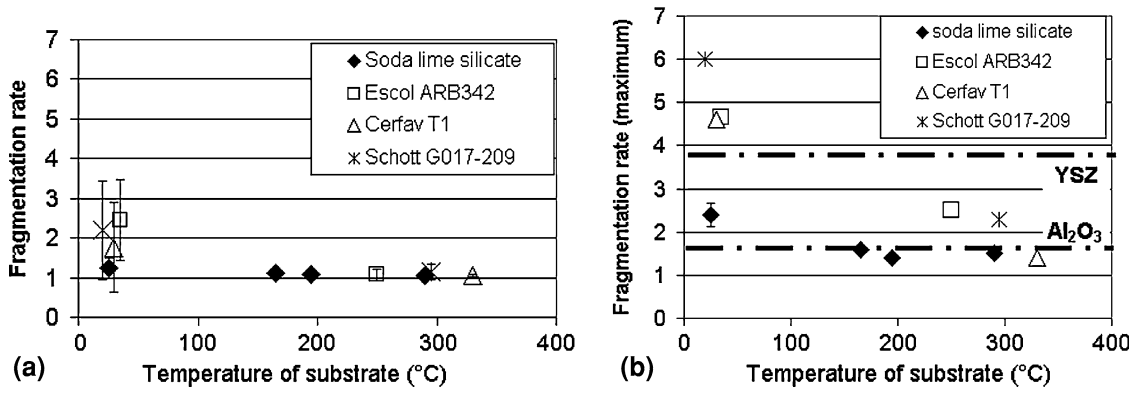


Fig. 3 Degree of fragmentation (F) of several glass compositions depending on substrate temperature (T_s): (a) median value, (b) maximum value, compared with maximum values of alumina (after Escure (Ref 30)) and YSZ (after Li et al. (Ref 50)) onto substrates at room temperature)

Table 4 Comparison of estimated cooling and flattening times, for given diameter and velocity conditions

Feedstock	Alumina	Soda lime silicate glass
t_{transf} (ns)	8-158	186-3518
t_{splat} (ns)	33-417	33-417
$\Xi = t_{\text{transf}} / t_{\text{splat}}$	0.24-0.40	5.3-8.8

of glass splats allows to study *a posteriori* their spreading mechanism, and to identify some effects that would be hardly observable with crystalline oxides.

3.3 Observation of Wavelets in the Glass Splats

3.3.1 Origin of Wavelets. When a splat remains fluid for a long time (i.e., as long as its temperature is above its

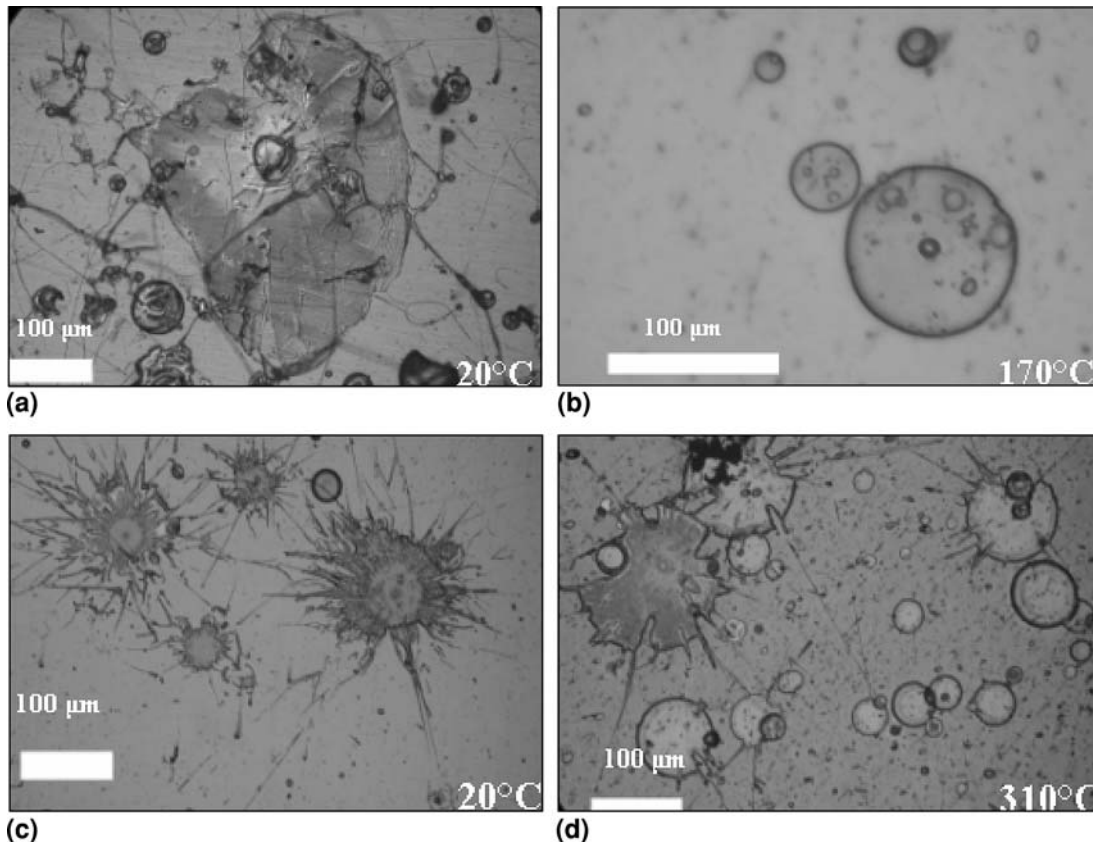


Fig. 4 Aspect of splats of (a, b) soda lime silicate glass and (c, d) Schott G017-209 (Zn-Pb-B) glass with substrate temperatures of (a, c) $T_s = 20$ °C, (b) $T_s = 170$ °C, and (d) $T_s = 310$ °C

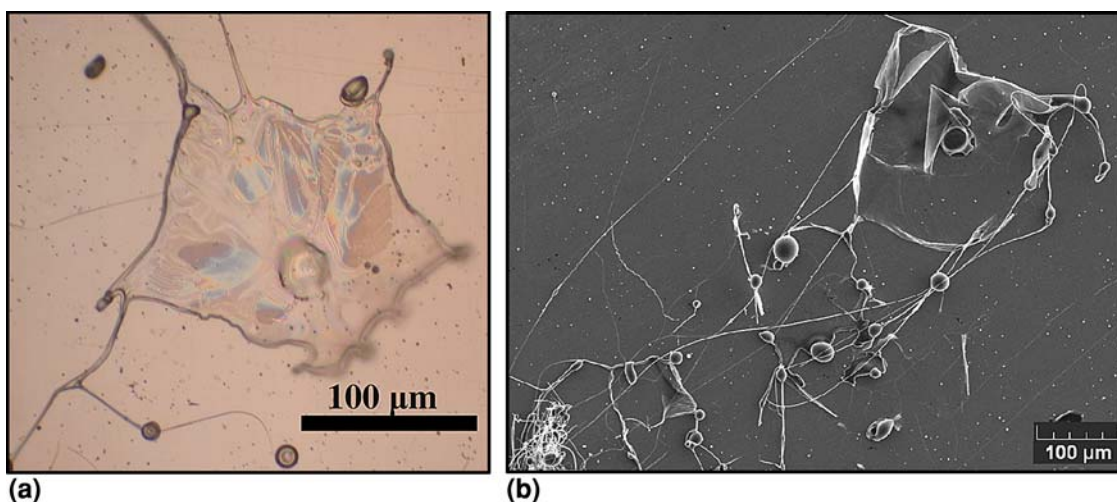


Fig. 5 Unmolten core and peripheric film: here: Cerfav Z5M splot ($T_s=20\text{ }^\circ\text{C}$) seen under optical microscopy (a) and SEM (b)

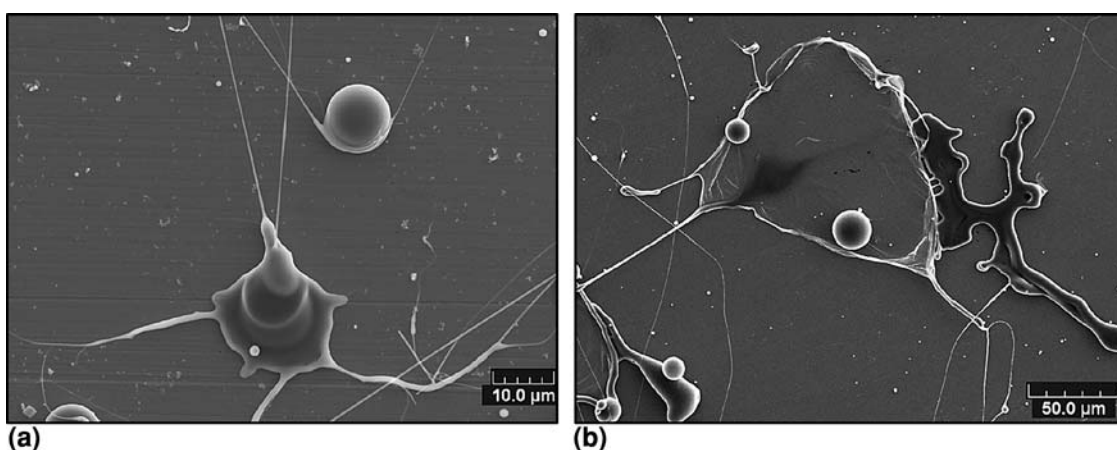


Fig. 6 (a) Fiberization of two objects and (soda lime silicate, $T_s=20\text{ }^\circ\text{C}$); (b) beginning coalescence of a recently flattened splot (right) with another splot (left) (Cerfav Z5M, $T_s=20\text{ }^\circ\text{C}$)

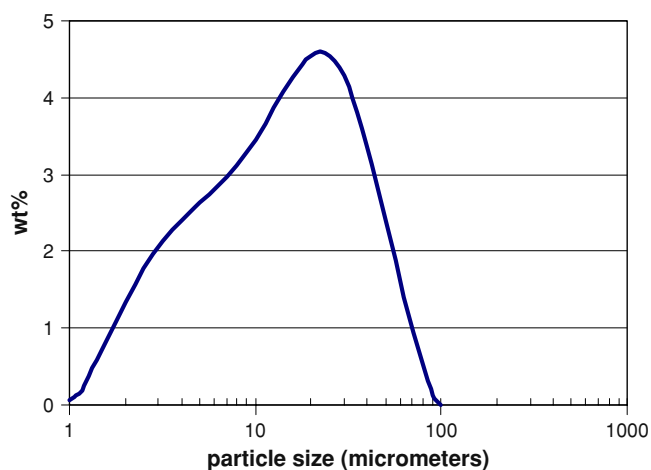


Fig. 7 Size distribution of Z5M glass powder

solidification temperature, T_{fusion} , for a crystalline oxide, T_g for a glass), the probability of the occurrence of a second particle impact at the same location (before the primary splot cools down) becomes not negligible. Of course, the determination of a precise value is quite difficult due to the evolution of splot size with time and also to surfusion aspects (Ref 4). Thus, in order to simplify the probability calculus, splats will be considered in the following as isothermal and fluid splats, which have their final surface area during all the lapse of time t_{transf} . During this lapse of time, a number N of particles will impinge onto a total exposed surface S_{exposed} . For this whole surface, the considered splot (surface area S_{splat}) will receive a part of these particles. Each impinging particle has a probability $P_{\text{contact 1particle}} = S_{\text{splat}}/S_{\text{exposed}} = 1 - P_{\text{non-contact}}$ of touching the studied splot. Thus, the global non-contact probability is $P_{\text{non-contact}} = [1 - S_{\text{splat}}/S_{\text{exposed}}]^N$ and the global contact probability is $P_{\text{contact}} = 1 - P_{\text{non-contact}}$. The value

of N depends on several factors: (a) the mass particle flow rate \dot{m} , (b) the powder volumetric mass, (c) the size distribution (a finer and lighter powder yields a higher value of N): $N = \frac{\dot{m}}{\rho} \cdot t_{\text{transf}} \cdot \sum_i \left[\frac{V_i}{\frac{4}{3}\pi d_i^3} \right]$. For example, a Z5M glass powder (2492 kg/m^3) with the size distribution described in Fig. 7, thermally sprayed with a 2 g/min flow rate over a $100\text{-}\mu\text{m}$ diameter splat ($t_{\text{transf}} = 2 \cdot 10^{-6} \text{ s}$), corresponds to $N = 700$ particles. If the exposed surface is $2 \times 2 \text{ cm}^2$, the contact probability will be 1.4% , i.e., 1 chance out of 70. This means a moderate but quite significant probability of observing this phenomenon. On the other hand, an alumina powder (much shorter cooling time) with the same size distribution and spraying conditions, would have $P_{\text{contact}} = 0.06\%$, i.e., 1 chance out of 1700. If commercial alumina ($22\text{-}45 \mu\text{m}$) were used, P_{contact} would decrease to 1 chance out of 200000.

3.3.2 Identification of the Secondary Impact Phenomenon. Some glass splats, such as the one displayed in

Fig. 8, show the presence of concentric wavelets. The distance between each wave from their center appear to be increasing, as shown in Fig. 9, and the waves are not visible on their rear front. This situation seems clearly to correspond to the impact of a secondary particle, which impinged onto the spreading splat, as glass was still hot and fluid. The profile of waves leads to conclude that the spreading velocity U of the splat was inferior to the wavelet speed c . The information given by the secondary impact could then supply a better knowledge of the local spreading velocity than the global estimation given by Schiaffino's (Ref 47) model, which suggests a median spreading velocity $U = V$ (here: $V = 270\text{-}300 \text{ m/s}$) only when c could be accurately estimated.

3.3.3 Estimation of Wavelet Speed. Kinematical Approach: the maximum value of c can be calculated as follows: $c = l/T$, T being the necessary time period to travel through the distance l ($\approx 1.5 \mu\text{m}$) between 2 successive wavelets. The observation of SEM picture (Fig 8) shows

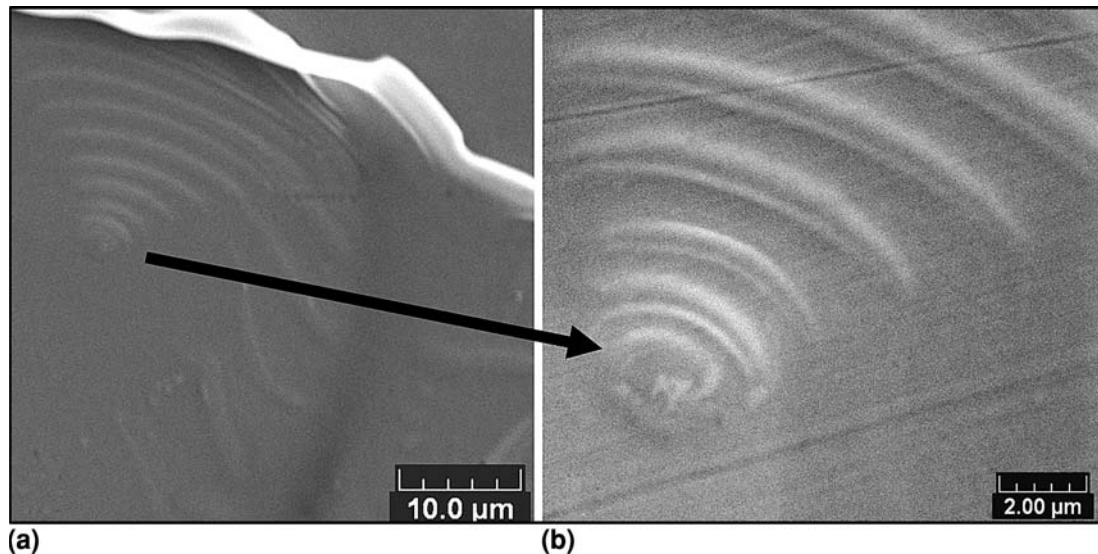


Fig. 8 Wavelets observed by SEM on a Cerfav Z5M splat

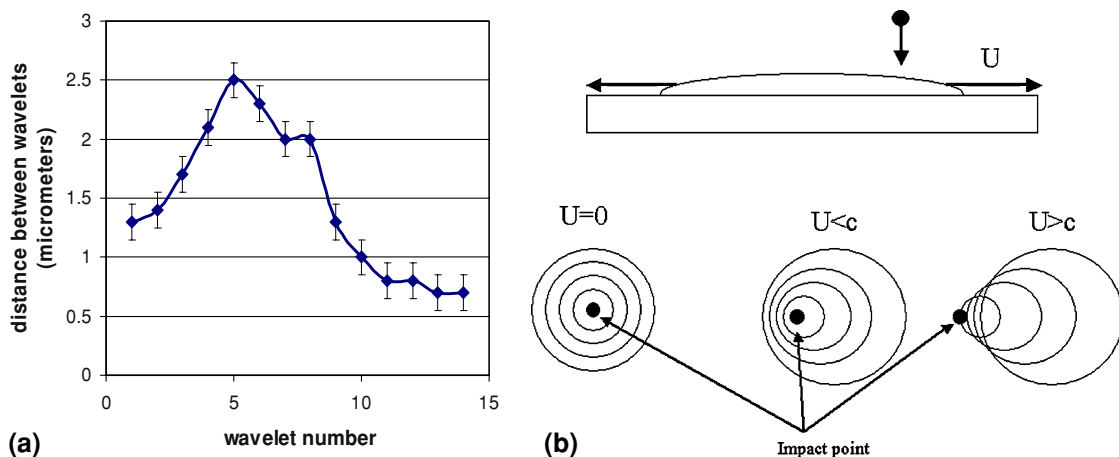


Fig. 9 (a) Distance between wavelets observed by SEM on a Cerfav Z5M splat, (b) identification of the phenomenon: $U < c$

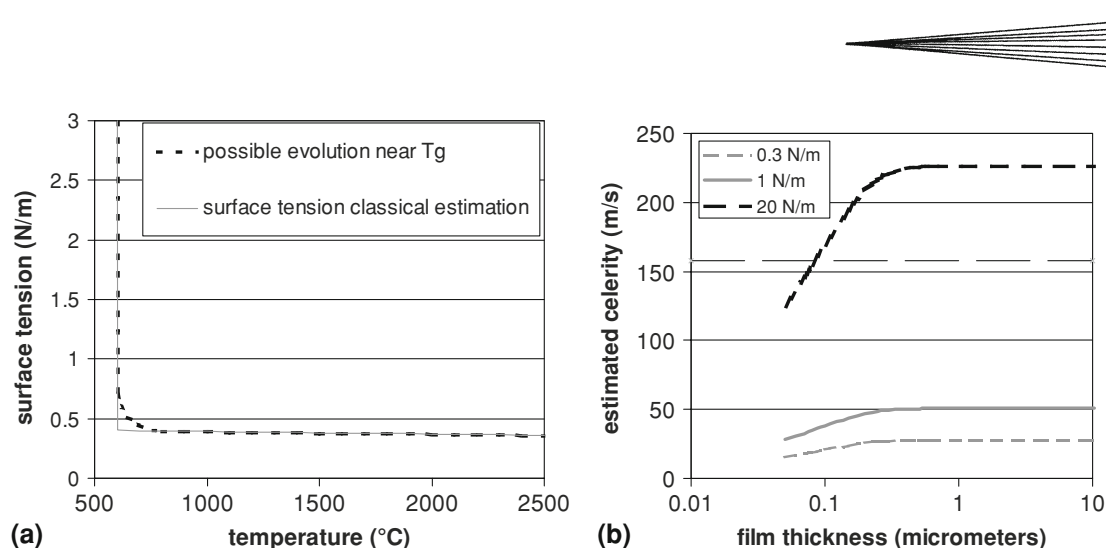


Fig. 10 (a) Suggested evolution of $\sigma(T)$ near T_g , and (b) subsequent evolution of wavelet speed versus film thickness assuming several values for surface tension

$n = 14$ wavelets, and a total travel distance $\mathcal{L} = 21 \mu\text{m} \approx n \cdot l$ between the impact point and the edge of the splat. It is to note that wavelets 13-14 are visible at the very edge of the splat, and that wavelets 8-14 present a harsh reduction of l , maybe because of a local thickness change. The necessary time to produce all these wavelets should be inferior to the estimated spreading time (t_{splat}), therefore:

$$n \cdot T \leq t_{\text{splat}} \text{ thus } T \leq t_{\text{splat}}/n \text{ and } c > n \cdot l/t_{\text{splat}} \quad (\text{Eq 4})$$

$$\approx \mathcal{L}/t_{\text{splat}} = \mathcal{L}/(D/V) = \mathcal{L} \cdot V \cdot \xi/D_{\text{splat}}$$

giving $c > 21 \cdot 10^{-6} \times 300 \times 2.5/100 \cdot 10^{-6} = 158 \text{ m/s}$. Under this kinematical point of view, the minimum speed can then be estimated. But this does not supply information about the local spreading velocity ($U < c$), which is only supposed to be inferior to the median velocity $U = V$ (Ref 47).

Hydrodynamic Approach: the similarity with the waves produced in a water film (G.B. Homsy, 2007, Personal communication; P. Belleudy, 2007, Personal communication; M. Rabaud, 2007, Personal communication), considering $c = l \cdot f = l \cdot \omega/2\pi$, yields:

$$\Omega = \sqrt{\left(g \cdot \frac{2\pi}{l} + \frac{\sigma}{\rho} \cdot \frac{8\pi^3}{l^3}\right) \cdot \tanh\left(\frac{2\pi \cdot e}{l}\right)} \quad (\text{Eq 5})$$

where $e =$ film thickness, $g =$ gravity constant.

The first term of the equation corresponds to the gravitational component of the waves, whereas the second term describes the capillary component. The former term is insignificant, since measured value of l (1-2 μm) is very inferior to $l_c = 2\pi\sqrt{(\sigma/(\rho \cdot g))} \approx 21000 \mu\text{m}$. This hypothesis is confirmed by the fact that this impact took place onto a vertical substrate. Thus, the studied phenomenon is strictly capillary. The density and surface tension of the glass are known (see Table 3: $\sigma \approx 0.3 \text{ N/m}$), therefore the only unknown value necessary to estimate ω would be the value of the film thickness e in the glass splat. According to the irisation effects seen in optical microscopy (see Fig. 5a), e is expected to have micrometric or

submicronic values. An evolution study with $50 \text{ nm} < e < 10 \mu\text{m}$ yields speed values c between 15 and 26 m/s (see Fig. 10). However, this result is much lower than the minimum value estimated by the kinematical approach. This fail of the hydrodynamic approach probably comes from the assumption of a completely isothermal fluid, with a constant and low surface tension. In fact, the surface of the flattening glass splat in contact with air has probably a higher surface tension than the calculated value at 2700-3000 °C. The glass transition phenomenon could allow the existence of a progressive increase of $\sigma(T)$ near T_g , instead of a first order increase when liquid (finite value $\sigma(T) \approx 0.3 \text{ N/m}$) acquires a “solid” behavior ($\sigma \rightarrow \infty$). The evolution of the estimated wavelet speed, supposing an external surface temperature near T_g , give values (Fig. 10) that are more compatible with the kinematical approach when the estimated surface tension is above 10 N/m. Thus, the difficulty of measuring the surface tension of glass near T_g makes it difficult to employ the hydrodynamical approach to estimate c . However, it seems to open interesting perspectives about the understanding of the hydrodynamics of glass and splats.

4. Conclusion

Glass transition and low-thermal conductivity allow glasses to cool down very slowly, which gives place to higher spreading and degree of fragmentation than for classical oxides, such as alumina. The predicted trends about splat formation, cooling, and fragmentation are confirmed by experimental results, and the effect of viscosity and surface tension, which can be controlled by choosing suitable glass compositions, allows modifying the splash-splat transition temperature. Peculiar morphological aspects were observed on glass splats, such as fiberization, unmolten core, peripheral thin films and post-splat coalescence. Wavelets caused by a secondary impact onto

a still spreading, fluid splat, were identified. The probability of observing these wavelets was compared between glass and alumina, suggesting that these observations are only possible on glass splats. Thus, thanks to its typical properties, glass allows to “freeze” some phenomena that are very difficult to visualize when crystalline oxides are used, and offers opportunities of deepening the knowledge of splat formation. From these observations, two methods to estimate the wave speed were proposed, opening interesting perspectives of calculating minimum velocity of the particle spreading on the substrate, even though better accuracy will be required in the knowledge of surface tension values near glass transition to achieve a suitable calculus.

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